

SPASSKAYA, R.I.; KAZARNOVSKIY, S.N.

Continuous method of producing guanidine from urea. Khim.prom.
no.7:488-491 J1 '63. (MIRA 16:11)

ANTIPINA, I. V.; KAZARNOVSKIY, S. N.; Prinimala uchastiy: LEBEDEVA
V. V.

Oxidation of cyclohexylamine by hydrogen peroxide to cyclohexanone
oxime. Khim prom no. 3:165-170 Mr '64. (MIRA 17:5)

MALKINA, N.I.; KAZARNOVSKIY, S.N.

Synthesis of cyanuric acid from urea. Zhur.prikl.khim. 37
no. 5:1158-1160 My '64.
(MIRA 17:7)

1. Gor'kovskiy politekhnicheskoy institut imeni A.A.Zhdanova.

L 10407-66

ACC NR:

EWT(m)/EWP(w)/EWP(j)/EWP(t)/EWP(b)
AM5022503

Monograph

JD/WB/DJ/ME/RM

UR/

Kolotukhin, Ivan Nikiforovich; Kuznetsov, Vasily Georgiyevich; Kazarnovskiy, Semen Naumovich; Tsaregradskiy, Vladimir Alekseyevich

Lubricating and protective materials (Smazochnyye i zashchitnyye materialy) 3d ed., rev. and enl. Moscow, Izd-vo "Transport," 1965. 171 p. illus., biblio., 8000 copies printed.

TOPIC TAGS: lubricant, lubricant component, lubricant property, lubricating oil, grease, lubrication, paint, lacquer, detergent, railway rolling stock, protective coating, corrosion protection

PURPOSE AND COVERAGE: This monograph presents the basic properties, test and preparative methods, and also applications for lubricant and protective paints and lacquers required in the railroad industry. Compared with the second edition, this edition provides additional information on synthetic oils, greases, new synthetic polymeric paints and lacquers, and also detergents and polishing compositions. The monograph was approved by the State Administration for Educational Institutions of the Ministry of Transport as a textbook for rail transport technical schools and can be used by a wide range of workers who are connected with painting and lubrication of rolling stock.

Card 1/3

UDC: 625.23/.24002.4:[621.892+66]
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SUB CODE: *FP, MT*/SUBM DATE: 25Mar65/ ORIG REF: 033

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Card 3/3

KOLOTUKHIN, Ivan Nikiforovich; KUZNETSOV, Vasilii Georgiyevich;
KAZARNOVSKIY, Semen Naumovich; TSAREGRADSKIY, Vladimir
Aleksseyevich; SARANTSEV, Yu.S., red.

[Lubricating and protective materials] Smazochnye i zashchit-
nye materialy. Izd.3., perer. i dop. [By] I.N.Kolotukhin,
i dr. Moskva, Transport, 1965. 171 p. (MIRA 18:4)

KAZARNOVSKIY, V.

[Analysis of the financial administration of industrial enterprises]
Analiz khoziaistvennoi deiatel'nosti promyshlennogo predpriiatiia.
Moskva, Gosfinizdat, 1954. 133 p. (MLRA 7:12)
(Industrial management)

Translation from: Referativnyy zhurnal, Geologiya, 1957, Nr 4, 15-57-4-5393
p 184 (USSR)

AUTHORS: Borisova, E. A., Kazarnovskiy, V. D.

TITLE: Laboratory Investigations on the Treatment of Saline Soil by Liquid Bitumen With Preliminary Flushing by Water (Laboratornyye issledovaniya po obrabotke zasolennykh gruntov zhidkim bitumom s predvaritel'noy promyvkoj)

PERIODICAL: Tr. Mosk. avtomob.-dor. in-ta, 1956, Nr 18, pp 241-248.

ABSTRACT: The material used was chloride-sulfate saline soil cut from a section of rock in the Andizhanskaya Oblast', Uz SSR. The data of the investigations are given. It was discovered that when the chloride and sulfate content of soil exceeds one percent, the soil is unsuitable for treatment with organic binding material in highway construction and demands preliminary flushing by water. The authors outline the relationship between number of flushings of the soil by water and the quantity

Card 1/2

Laboratory Investigations on the Treatment of Saline (Cont.) 15-57-4-5393

of indroducible bitumen. They show the possibility of lowering the quantity of binding substance by increasing the number of flushings, and, on the other hand, lowering the number of flushings by somewhat increasing the expenditure of binding substance, depending on the economy of the construction. It is noted that flushing of the soil has not yet been applied in highway-construction practice. However, flushing the soil before treating with liquid bitumen may prove to be much more profitable than replacing the saline soil. The results obtained from testing samples by composite flushing of soil and use of liquid bitumen (bulk weight, water saturation, swelling, durability of dry and capillary-moistened samples) are in agreement, according to the degree of fitness of saline soils, with the classification of the "Technical rules on the construction of a roadbed and highway base in the desicated zone on saline soils." Flushing of the soil (2 to 3 times) is proposed for the roadbed immediately next to the highway. For flooding sections of the earthen roadbed, it is necessary to construct retaining borders of planking or of low soil ridges.

Card 2/2

Ye. G. B.

KAZARNOVSKIY, V.D., inzh.; KAZARNOVSKAYA, E.A., inzh.

Washing salty soils for road construction. Trudy MADI no.22:
170-175 '58. (MIRA 12:4)
(Soil physics) (Road construction)

KAZARNOVSKIY, Vladimir Davydovich; GANYUSHIN, A.I., red.; MAL'KOVA,
N.V., tekhn. red.

[Calculation of the shear strength of soil in the designing of
a road] Uchet soprotivliaemosti grantov sdvigu pri proektirova-
nii dorozhnoi konstruktsii. Moskva, Avtotransizdat, 1962. 34 p.
(MIRA 15:5)

(Soil mechanics)

(Roads--Designing)

KAZARNOVSKIY, V.D., inzh.

Degree of soil stabilization and the shear resistance of ground.
Avt.dor. 24 no.12:15-17 D '61. (MIRA 14:12)
(Soil stabilization)

MASLOV, N.N., prof., doktor tekhn.nauk, zaslushennyi deyatel' nauki i
tekhniki FSFSR; KAZARNOVSKIY, V.D., inzh.

Using the density-humidity method in determining soil
resistance. Avt.dor. 25 no.12:19-21 D '62. (MIRA 16:2)
(Soil mechanics)

FUZAKOV, N.A., doktor tekhn. nauk; KHARKHUTA, N.Ya., doktor tekhn. nauk; KOTILEV, Yu.L., kand. tekhn. nauk; VEYIZHAN, M.I., kand. tekhn. nauk; MITASOV, I.V., inzh.; LEVITSKIY, Ye.F., inzh.; RUMANOV, A.Z., inzh.; Primali uchastiye: LAZARENKOVSKIY, Y.D., kand. tekhn. nauk; DENISOV, Ye.M., inzh.; TOPOL'NITSKAYA, L.F., red.

[Instruction for building earth automobile roadbeds! Instruktsiya po sooruzheniiu zemlianoego polotna avtomobil'nykh dorog (VSM 97-63). Moskva, Transport, 1964. 238 p.

(MIRA 17:11)

1. Russia (1923- U.S.S.R.) Gosudarstvennyy proizvodstvennyy komitet po transportnomu stroitel'stvu.

KAZARNOVSKIY, Ya. S.

"The Explosive Conversion of Methane, Part 1", Khimicheskaya
Pererabotka Neftnykh Uglevodorodov (Chemical Conversion of Petroleum
Hydrocarbons), Academy of Sciences USSR, Moscow, 1956, pp 133-141

541, 1424

KAZARNOVSKIY, Ya. S.

"The Explosive Conversion of Methane, part 2", Khimicheskaya
Pererabotka Neftyanykh Uglevodorodov (Chemical Conversion of Petroleum
Hydrocarbons), Academy of Sciences USSR, Moscow, 1956, pp 142-152

544, 1424

KAZARNOVSKIY, Ya. S.

"The Explosive Conversion of Methane; Part 2," Khimicheskaya
Pererabotka Neftnykh Uglevodorodov (Chemical Conversion of Petroleum
Hydrocarbons), Academy of Sciences USSR, Moscow, 1956, pp 153-166

Sum 11/29

CO

2

PROCESSES AND PROPERTIES INDEX

Calculation of the composition of the gas phase above a binary solution. I. R. Krichvskii and Ya. S. Kazar-novskii, *J. Phys. Chem. (U. S. S. R.)* 9, 1222-9 (1934); cf. *C. A.* 29, 1704^h.—By means of a numerical integration of the Gibbs-Duhem equation in the form $dx_1 = x_1(1 - x_1)/P(x_1) - NP$ by the method of Runge the gas-phase compn. is calcd. as a function of the molar compn. of the liquid and the resp. vapor pressures. At 35.17° in $\text{Me}_2\text{CO}-\text{CS}_2$ solns. some values of the mol. fraction of Me_2CO in the liquid, the mol. fraction calcd. and that found in the gaseous state were 0.9376, 0.734, 0.749; 0.7185, 0.448, 0.428; 0.5540, 0.283, 0.298; 0.2762, 0.322, 0.312, 0.0308, 0.116, 0.110. By applying the Lewis-Randall concept of fugacity and the Hines and Clark value (*C. A.* 26, 3172) for polymerization of HOAc , (selected) mol. fractions of HOAc in HOAc - PhMe solns. at 80.115° gave the calcd. and found mol. fractions of HOAc in the gaseous state: 0.9830, 0.940, 0.937, 0.7513, 0.631, 0.612; 0.5501, 0.502, 0.485. In $\text{HOAc}-\text{H}_2\text{O}$ solns. at 80.00°, some values were, resp.: 0.8781, 0.760, 0.770; 0.6404, 0.458, 0.433; 0.2205, 0.179, 0.169, 0.0630, 0.0603, 0.0439. F. H. R.

ASB-SLA METALLURGICAL LITERATURE CLASSIFICATION

83000 STUDIES

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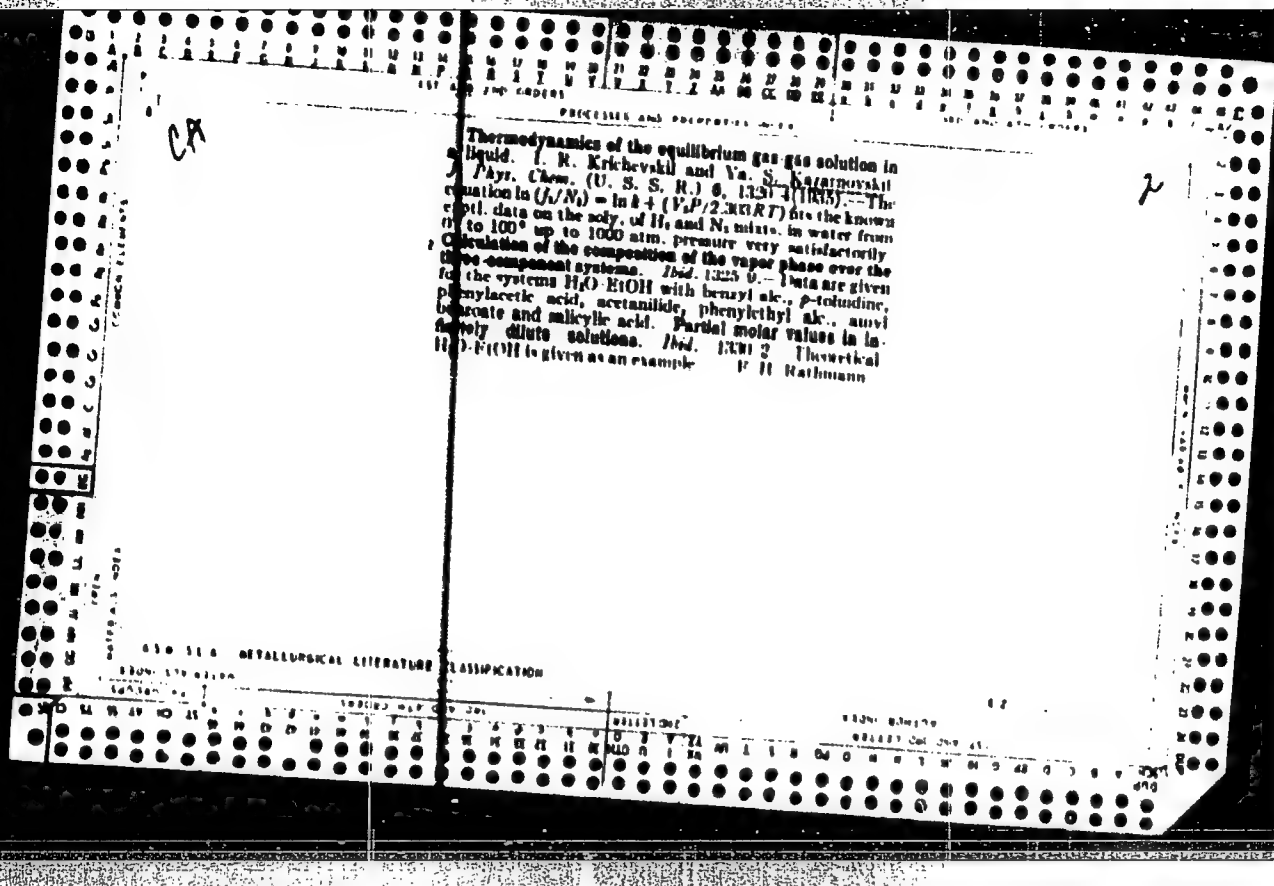
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| 1ST AND 2ND CODES | | PROCESS AND PROPERTIES INDEX | | 3RD AND 4TH CODES | |
|---|--|------------------------------|--|-------------------|--|
| <p>BC</p> <p>Explosive oxidation of methane. N. KOSOV, J. KASAROVICH, and L. KASOVICH (Acta Physico-chem. URSS, 3, 867-878).—The yield of CO_2, H_2O, CO, and H_2 per cu.m. of CH_4 consumed in an equimol. mixture of CH_4 and O_2 is independent of pressure up to 8-70 atm. and is unaffected by the nature of the wall or the diameter of the vessel, although the amount of CH_4 oxidized is less in narrow vessels. The influence of additions of N_2, CO, CO_2, and H_2 is in agreement with thermodynamic requirements. The explosion temp. calc. from the water-gas equilibrium data agrees closely with that calc. from sp. heat data, and it is inferred that equilibrium is attained in the explosion. If H_2O is present initially CH_2O and EtOH are formed and equilibrium is not attained. The reaction forms a suitable source of H_2 for the NH_3 synthesis. R. S.</p> | | | | | |
| <p>ASS-SLA METALLURGICAL LITERATURE CLASSIFICATION</p> | | | | | |
| <p>1900: 571819</p> | | | | | |
| <p>1900: 571819</p> | | | | | |

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| <p>Calculation of dipole moments. I. R. Krichevskii and Ya. S. Kabanovskii. <i>J. Phys. Chem. (U. S. S. R.)</i> 6, 839-41(1969).—Theoretical and review. Various equations are discussed with examples of exper. data from the literature. An equation applying the methods of dipole moments is derived and found in many cases to be more satisfactory than that of Debye. P. H. Rathmann</p> | | | | | |
| <p>ASACSLA METALLURGICAL LITERATURE CLASSIFICATION</p> | | | | | |



| 1ST AND 2ND ORDERS | | | | | | | | | | | | | | | | | | | | | | | | | | 3RD AND 4TH ORDERS | | | | | | | | | | | | | | | | | | | | | | | | | |
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| PROCESSING AND PROPERTIES INDEX | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| <p>CA</p> <p>18</p> <p>Obtaining hydrogen and hydrogen-nitrogen mixtures by the explosive oxidation of methane. N. I. Kobzarev.</p> <p>Yu. S. Katsimovskii and L. I. Kashtanov. <i>J. Chem. Ind. (Moscow)</i> 12, 1030-6 (1935).--The explosion of equimol. amts. of CH_4 and O_2 gives a yield of 37.8% CO and 49.4% H_2, i. dependent of pressure from 0.72 to 3.7 atm. The walls of the reaction vessel had no effect, but reduction of the diam. of the vessel hinders the reaction without changing the final products. Addn. of N_2 to the mixt. lowers the yield of CO and H_2 somewhat, but this effect can be counteracted by the presence of CO_2. Addn. of H_2O to the mixt. causes incomplete reaction. Calculs. show that the temp. conditions of the reaction probably det. purely thermodynamically the direction of the explosion.</p> <p>H. M. Tolstouk</p> | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| <p>ASB-SLA METALLURGICAL LITERATURE CLASSIFICATION</p> | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |

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PROCESSES AND PROPERTIES INDEX

H-1

Free energies of formation of sodium carbonate and hydrogen carbonate. I. R. KATTSCHENSKI and J. S. KASARKOVSKI (J. Phys. Chem. Russ., 1937, 9, 688-690).—The free energy of formation (ΔF) of Na_2CO_3 is calc. (a) from the sum of changes in F corresponding with eight partial reactions, and (b) from the third law of thermodynamics. The vals. obtained are $\Delta F_{\text{exp}} = -240.6$ kg.-cal. (a) and -251.8 kg.-cal. (b). The corresponding vals. for NaHCO_3 are -203.2 and -204.3 kg.-cal. For the reaction $2\text{NaHCO}_3 \rightarrow \text{Na}_2\text{CO}_3 + \text{H}_2\text{O} + \text{CO}_2$, $\Delta F_{\text{exp}} = 2.0$ kg.-cal. (calc.), compared with 2.5 kg.-cal. (exp.).
E. R.

ASB-51A METALLURGICAL LITERATURE CLASSIFICATION

| SOURCE SYNOPTIC | | | | | | | | | | SOURCE ABSTRACT | | | | | | | | | |
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CA

PROCESSES AND PROPERTIES INDEX

2

The calculation of solubility in ternary systems. Ya. S. Masarnovskii. *J. Phys. Chem. (U. S. S. R.)* 10, 25-31 (1937). — For ternary systems composed of 2 volatile and 1 nonvolatile component the equation $n_1 \Delta n_1 / \Delta n_1 + n_2 \Delta n_2 / \Delta n_2 + n_3 \Delta n_3 / \Delta n_3 = 0$ is prepared for calcg. the soly. of the nonvolatile phase. With Avdeeva's data (C. A. 34, 4122) there is good agreement between expl. and calcd. values. F. H. Rathmann

ASB-SLA METALLURGICAL LITERATURE CLASSIFICATION

| FROM SYMBOL | SYMBOLS AND ONLY ONE | COLLATIONS | SYMBOLS AND ONLY ONE |
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| PROCESSING AND PROPERTIES INDEX | | | | | | | | | | | | | | | | | | | |
| <div style="display: flex; justify-content: space-between;"> CA 2 </div> <p>An equation of state for gaseous mixtures. I. R. Krichevskii and Ya. B. Kamenovskii. <i>Acta Physicochim.</i> U. R. S. S. 10, 317-44 (1950) (in English).--Data on the P-V-T relations for various A-C₂H₄, O₂-C₂H₄, air, N₂-CH₄, N₂-NH₃, pure H₂ and H₂-CO mixts. at 0 to 300° and at pressures up to 1000 atm. are given. In the equation $p = p_1^0 N_1 + p_2^0 N_2 + a N_1 N_2 (p_1^0 - p_2^0)$, a has the values 0.474 for A-C₂H₄ at 25° up to 125 atm.; 0.523 for N₂-O₂ (air) from 0 to 300° and up to 3700 atm.; 0.520 for O₂-C₂H₄ at 25° up to 125 atm.; 0.464 for N₂-CH₄ from 0 to 200° and up to 25 atm.; 0.519 for N₂-H₂ at 0° up to 1000 atm., and 0.465 at 300°; 0.741 for H₂-CO at 0-25° and up to 600 atm. The data also obey the fugacity equation $RT \ln (f_1/p_1^0) = N_1 RT \ln (f_1/p_1^0) + N_2 (1 + a - (N_1 - N_2)(p_1^0 - p_2^0))$, where f_1 and f_2 are the fugacities and N_1 and N_2 the mole fractions to within a max. error of ca. 6% and a mean square error of ca. 1%.</p> <p style="text-align: right;">P. H. Rathmann</p> | | | | | | | | | | | | | | | | | | | |
| 458.514 METALLURGICAL LITERATURE CLASSIFICATION | | | | | | | | | | | | | | | | | | | |
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1ST AND 2ND EDITIONS
 PROCESSES AND PROPERTIES INDEX
 1ST AND 2ND EDITIONS

& PAZARNOVSKIY YA.S. H-1

Equation of state for gas mixtures. I. R. KRIVONOSHI and J. N. KARABAYSKI (J. Phys. Chem. Russ., 1939, 13, 376-396).—A semi-empirical equation for the total pressure, p , of a binary gas mixture is proposed: $p = p_1 N_1 + p_2 N_2 + a N_1 N_2 (p_1 - p_2)$, where p_1 and p_2 are the pressures of the components for a vol. equal to the mol. vol. of the mixture, N_1 and N_2 the mol. fractions of the components, and a is a const. which can be a function only of the temp. (cf. A., 1938, I, 611). It agrees with existing data for a wide range of temp., pressure, fugacity, and composition. R. C.

State Ind. of Nitrogen Industry, Moscow

A.S. 51.4 METALLURGICAL LITERATURE CLASSIFICATION

1ST EDITION
 2ND EDITION

1ST EDITION
 2ND EDITION

Compressibility of ammonia at high temperatures and pressures. Ya. S. Kazarnovskii. *Acta Physicochim. U. R. S. S. 12, 513-23 (1940)*. P-V values are given for 25° intervals from 200° to 300° and for pressures 100 to 1000 atm. The values are correct to 0.5%. H. C. P. A.

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|--|--|-------------|--|
| STANDARD AND PAPER-DRIVEN INDEX | | 2 | |
| <p>Equation of state for gas mixtures. Ya. S. Kazarnovskii. <i>Acta Physicochim. U. R. S. S. R.</i> 13, 833-73 (1945) (in German); cf. C. A. 33, 6108. The equation of state for binary gas mixts. $p = p_1 N_1 + p_2 N_2 + a N_1 N_2 (p_1 - p_2)$ was developed. The components of the mixt. are dipoles with rectilinear isometrics, and the coeff. a is a temp. function. The dependence of the function a on temp. was shown experimentally with the binary gas mixts. NH_3-H_2 and NH_3-N_2. The equation gave satisfactory results for the compressibility of the gas mixts. over a wide range of temp. and pressure. For ternary gas mixts. $p = p_1 N_1 + p_2 N_2 + p_3 N_3 + a_{12} N_1 N_2 (p_1 - p_2) + a_{13} N_1 N_3 (p_1 - p_3) + a_{23} N_2 N_3 (p_2 - p_3)$ reproduced the exper. data for the compressibility of mixts. of $N_2-H_2-NH_3$. The binary gas-mixt. equation was successfully applied to the exper. data for binary mixts. of H_2 and N_2 in liquid NH_3. W. George Parks</p> | | | |
| ASB-51A METALLURGICAL LITERATURE CLASSIFICATION | | | |
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| 10000 00 | | 10000 00000 | |

Compressibility of nitrogen-hydrogen-ammonia mixtures at high pressures and temperatures. Ya. S. Kargin, N. N. Novikova, G. N. Simonov and G. R. Arlovsk. *Dokl. Akad. Nauk SSSR*, (U. S. S. R.) 14, 774-81 (1940); (J. C. C. 36 2168). The compressibility of two H_2 - N_2 and one H_2 - NH_3 and three H_2 - N_2 - NH_3 mixts. was measured at 50, 200°, 250° and 300°, up to 1640 atm. By use of these values and the Beattie-Bridgman equation, the mol. vols. were calcd. with a possible error of 1%. H. C. P. A.

ASS-56A DETALLURGICAL LITERATURE CLASSIFICATION

8C

Equation of state for gas mixtures. J. S. Krasovskii (*Phys. Chem. Russ.*, 1945, 14, 1445-1447). If all the pressures are given for the same mol. vol., the pressure of a mixture $p = p_1 N_1 + p_2 N_2 + \dots + p_n N_n$ (p_1, p_2, \dots, p_n and N_1, N_2, \dots, N_n being the pressures and mol. fractions of the first component, and a a const. In non-polar mixtures a is independent of temp.; in polar mixtures it depends on temp. but is independent of N_1 . The equation can also be applied to mixtures of a gas and a saturated vapour, e.g., to p of H_2 and NH_3 over liquid NH_3 . An analogous equation is valid for ternary mixtures. J. J. B.

ASB SLA METALLURGICAL LITERATURE CLASSIFICATION

65

2

Effect of pressure on the heat of formation of ammonia.
 Ya. S. Kazarnovskii and M. Kh. Khatap'tyants. *J. Phys. Chem.* (U. S. S. R.) 15, (no. 73) (1941); cf. C. A. 35, 4104. The relation found by Gillespie and Beattie (C. A. 25, 242, 4172) using the Beattie-Bridgman equation for the heat of formation of NH_3 as a function of the pressure is incorrect. The equation for the heat capacity and compressibilities are not applicable. The values of Kowalevskii (C. A. 20, 7135) are similarly incorrect because the values obtained for the compressibilities by use of the van der Waals equation differ from expl. values by as much as 50 to 100%. The effect of pressure on the heat of the reaction $\frac{1}{2}\text{N}_2 + \frac{3}{2}\text{H}_2 = \text{NH}_3$ (all gases) at temps. from 250 to 500° and pressures up to 7000 atm. can, however, be calcd. by means of the equation: $\Delta H_p = \Delta H_{p=1} + \int_1^p \Delta \alpha dp - T \int_1^p (\Delta \alpha / \Delta T) dp$ and assuming that expl. values for the compressibility of NH_3 up to 300° can be extrapolated to 500°. At high temps. and pressures the heat effect is about 20% greater than at atm. pressure. The heats of mixing of H_2 and N_2 to form the three-component system H_2 - N_2 - NH_3 are calcd. by use of the Krichevskii-Khasanova equation (cf. preceding abstr.).
 P. H. Rathmann

ASD-55A DETAILING LITERATURE CLASSIFICATION

2

Thermodynamic properties of compressed ammonia.
 Ya. S. Kargin and Al. Kh. Karapet'yan. *J. Phys.*
Chem. (U.S.S.R.), 19, 173-80 (1943); cf. *C.A.B.*, 38, 5594.
 Fugacity, heat capacities, entropy, internal energy, free
 energy, etc., of NH_3 are calcd. from literature data for
 150-370° and 20-1000 atm. B. A.

Moscow State Nitrogen Inst.
 Order Lenin Chemical-Technological Inst. im. Mendeleev

ASB-SLA METALLURGICAL LITERATURE CLASSIFICATION

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| <div style="display: flex; justify-content: space-between;"> 1ST AND 2ND COPY 3RD AND 4TH COPY </div> <div style="display: flex; justify-content: space-between; align-items: center;"> CA PROCESSED AND REPRODUCED INDEX 2 </div> | | | | | | | | | |
| <p>Equation of state for gas mixtures. Ya. S. Kazarnovskii. <i>J. Phys. Chem. (U.S.S.R.)</i> 18, 304-70(1944). Math-theoretical. On the basis of equations of state for gases as developed by K. and Krichevskii (<i>C.A.</i> 33, 6104²), equations are derived for calcs. of internal energy, heat capacity, entropy, free energy, C_p, and differential throttling effect for binary and ternary gas mixts. Equations are also drawn for calcs. of partial molar quantities in these mixts. Thermal data on N-H mixts. correspond well to the calcd. amts. O. M. Kowolapoff</p> | | | | | | | | | |
| <div style="display: flex; justify-content: space-between;"> ASB-SEA METALLURGICAL LITERATURE CLASSIFICATION ENTRUSTMENT </div> | | | | | | | | | |
| <div style="display: flex; justify-content: space-between;"> 10000 02 10000 02 10000 02 10000 02 </div> | | | | | | | | | |
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| PROCESS AND PROPERTIES INDEX | |
|------------------------------|--|
| 1345. | <p>COMPRESSIBILITY OF METHANE AND METHANE-AMMONIA MIXTURES AT HIGH TEMPERATURES AND PRESSURES. Kazarnovskii, Y. S. and Levchenko, G. I. (J. Phys. Chem. (U.S.S.R.) 1944, 18, 380-2; U.O.P. Res. Lab. Abstr. 13 Feb. 1946, 21, 28) The compressibility of methane under pressures of 86.6 to 1400 atm. was determined at 250 and 300° C. The data at 200°C. agree well with those observed at low pressures by Kvalnes and Gaddy, while some discrepancies were observed at 250 and 300° C. For determination of the compressibility of methane-ammonia mixtures the method of Michels was used. The binary mixtures contained respectively 32.84, 39.58, 53.85 and 55.72 per cent ammonia. The pressures used ranged from 82 to 1675 atm. and the temperatures from 150 to 300°C. The isometric graphs of the binary mixtures are straight lines within a wide interval of temperatures and pressures, which allows reliable extrapolation of these data to higher temperatures. The data obtained are quite satisfactorily represented by the equation of state for binary gaseous mixtures derived by Krichevskii and Kazarnovskii.</p> |

~~RESTRICTED~~

KAZARNOVSKIYI, YA. S.

KRICHEVSKIYI, I. R., KAZARNOVSKIYI, YA. S., and
LEVCHENKO, G. T. (Nitrogen Inst. Moscow)
J. Phys. Chem. (USSR) 19, 314-22 (1945)
Thermodynamic properties of compressed nitrogen-
hydrogen mixtures.

~~RESTRICTED~~

Thermodynamic properties of nitrogen hydrogen ammonia mixtures. V. A. K. Kozlovskii (State Inst. Nitrogen Industry, J. Phys. Chem. 19, 382-404 (1945). For the mixt. NH_3 , 17.0, N_2 , 30.0, H_2 , 53.0%, the values of d log p/d log T , free energy, max. work, heat content, internal energy, and the two heat capacities are calculated for the temp. range 150-300° between 50 and 1000 atm. From the heat-content data for the mixt. and its constituents the heat of mixing of NH_3 with $\text{N}_2 + 3 \text{H}_2$ is calculated. If the heat of mixing is taken into account, the effect of pressure on the heat of NH_3 synthesis appears almost eliminated; the heat of reaction at 500° and 1000 atm. is only 3.4% higher than at the atm. pressure.

A16 314 METALLURGICAL LITERATURE CLASSIFICATION

| COMMON ELEMENTS | | | | | | | | | | COMMON VALENCE INDEX | | | | | | | | | |
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| 100 AND 41W INDEX | | | | | | | | | | 100 AND 41W INDEX | | | | | | | | | |
| <p>B</p> <p>Compressibility of Gases at High Pressures and Low Temperatures. (In Russian.) Ya. S. Kazarnovskii and I. P. Sidorov. <i>Zhurnal Fizicheskoi Khimii</i> (Journal of Physical Chemistry), v. 21, Nov. 1947, p. 1363 1370.</p> <p>Gives details of new and accurate method for determination of the above. Includes diagrams of apparatus. Compressibilities of hydrogen between 200 and 1805 atm. and between 0° and -84.9°C. were determined with an accuracy of 0.3-0.5%. 11 ref.</p> | | | | | | | | | | | | | | | | | | | |
| <p>ASPH-51A METALLURGICAL LITERATURE CLASSIFICATION</p> | | | | | | | | | | | | | | | | | | | |
| 100 AND 41W INDEX | | | | | | | | | | 100 AND 41W INDEX | | | | | | | | | |

KAZARNOVSKIY, Ya.S., kand.khim.nauk; SIDOROV, I.P., kand.tekhn.nauk;
KAZARNOVSKAYA, D.B., kand.khim.nauk

Equilibrium of homogeneous gas reactions at high pressure.
Trudy GIAP no.7:21-25 '57. (MIRA 12:9)
(Phase rule and equilibrium) (Gases)

KOBOZEV, N.I., doktor khim.nauk; KAZARNOVSKIY, Ya.S., kand.khim.nauk;
MENDELEVICH, I.I., kand.technik.nauk

Explosive conversion of methane. Part 1. Trudy GIAP no.7:
155-166 '57. (MIRA 12:9)
(Methane) (Oxidation)

KAZARNOVSKIY, Ya.S., kand. khim. nauk; DEREVYANKO, I.G.; STEZHINSKIY, A.I.
LOBZEV, N.I., doktor khim. nauk

Explosive conversion of methane. Part 2. Trudy GIAP no.8:89-105
'57. (MIRA 12:9)

(Methane) (Gas and oil engines) (Fuel--Testing)

KAZARNOVSKIY, Ya.S., kand.khim.nauk; KOBOZEV, N.I., doktor khim.nauk;
STREZHINSKIY, A.I.; TORBAN, B.S.

Explosive conversion of methane. Part 3. Trudy GIAP no.8:106-123
'57. (MIRA 12:9)

(Methane) (Gas and oil engines) (Fuel--Testing)

KAZARNOVSKIY, Ya.S.; KARKHOV, N.V.

High-temperature conversion of gaseous hydrocarbons. Biul. tekhn.-
ekon. inform. no.8:12-14 '58. (MIRA 11:10)
(Hydrocarbone)

APPROVED FOR RELEASE: 06/13/2000 P.; CIA-RDP86-00513R000721330005-0"

KAZARNOVSKIY, Ya.S.; KARKHOV, N.V.;
SOLNITSOVA, L.N.

Oxidative thermal pyrolysis of hydrocarbon gases to acetylene.
Khim. prom. no. 7:547-551 O-N '60. (MIRA 13:12)
(Hydrocarbons) (Acetylene)

SEMEV, V.P.; KAZARNOVSKIY, Ya.S.

High temperature conversion of individual hydrocarbons and
their mixtures. Gas.prom. 5 no.3:33-40 Mr '60.
(MIRA 13:6)

(Gases--Analysis) (Hydrocarbons)

KAZARNOVSKIY, Ya.S.; SEMENOV, V.P.

High-temperature conversion of hydrocarbons. Gaz.prom.
5 no.7:41-50 '60. (MIRA 1347)
(Hydrocarbons) (Oxidation)

S/064/61/000/001/002/011
B110/B215

AUTHORS: ~~Kazarnovskiy~~, Ya. S., Semenov, V. P., Ovcharenko, B. G.,
Tsypin, A. N., Kolodeyev, I. P., Litvinchuk, V. A.

TITLE: Problems of apparatus design for the thermooxidative pyrolysis
of hydrocarbon gases

PERIODICAL: Khimicheskaya promyshlennost', no. 1, 1961, 11-15

TEXT: The pyrolysis of hydrocarbon gases for the production of C_2H_2 and
synthesis gas takes place at 1450-1500°C. Since the intermediate C_2H_2 must
not remain in the reaction zone for more than 0.003-0.01 sec, short tongues
of flame must be used. As the traditional apparatus by Sachse and Bartho-
lomé with maximum production of C_2H_2 of 3500-5000 tons per year is no longer
sufficient, a new more efficient apparatus has to be designed. Highly turbu-
lent combustion increases the rate of flame propagation and shortens the
tongue considerably. The method of methane pyrolysis applied by B.S.Grinenko
yielded high C_2H_2 concentrations. Its industrial application, however, is

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Problems of apparatus design for...

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rendered difficult due to the almost critical velocity of the gas of 200-250 m/sec required for it, due to the high initial temperature (700-800°C) of the oxygen necessary for the combustion stabilization (7% of the total amount), and due to an increase in temperature of the reaction channel of up to 2000°C. A pilot plant for average gas velocities and efficiencies of approximately 160 Nm³/hr is described. The conical ring nozzle of the burner contained whirl blades. The CH₄/O₂ mixture flowed into the reaction channel at 400°C and approximately 150 m/sec. The oxygen used for stabilization was only 5% of the total O₂ content. Maximum temperature in the reaction zone was 1450°C; gas velocity: approximately 100 m/sec; its stay: 0.0025 sec. The acetylene yield was 8 to 8.4% of the reaction gases plus deposition of carbon black; 3 to 3.5 g/Nm³ of the initial mixture; ratio O₂ consumption = 0.62 to 0.64. According to the author, transition from pilot stage to industrial stage would be most suitable by increasing the number of burners. Fig. 1 shows the pilot plant of 1958. Coke oven gas of the ammonia unit compressed up to 0.36 atm by compressor (4), is purified in cloth filter (5),

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Problems of apparatus design for...

and conveyed to the preheating oven (3). Industrial oxygen compressed up to 0.38 atm by a $\chi K -3$ (ChK-3) compressor 1 is also conducted into the preheating oven via water separator (2) and filter (5). There, O_2 is heated to $350^{\circ}C$, and the coke oven gas to $450^{\circ}C$. From mixer (6), the mixture is at a temperature of $300^{\circ}C$ conducted into burner (7) and reaction vessel (8) from which the pyrolysis gases flow out at $80-90^{\circ}C$. After leaving scrubber (13) where the latter were purified from carbon black, they pass the water separator and filter before they are used for the production of acetylene. The triple burner of Fig. 3 which is used by the authors, has four spirals for producing whirls. Stabilizing O_2 is conducted through their axles. The

following parameters have to be observed exactly to attain an optimum course of reaction: consumption of O_2 and hydrocarbon gas, temperature of preheating, ratios $[O_2] : [\sum C_1]^2$ in the initial mixture, and amounts of water.

The following control and regulation apparatus were used: $\Delta \Pi M -270$ (DPM-270), $\Delta \Pi -410$ (DP-410), $\Delta \Pi -280$ (DP-280), $M(\Pi -\Pi p -54$ (MSSH-Pr-54), $\Xi \Pi \Pi -09$ (EPP-09), and $2 \Pi \Pi :24 \beta$ (2RL:24V) on AYU(AUS) blocks. The following average composition

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Problems of apparatus design for...

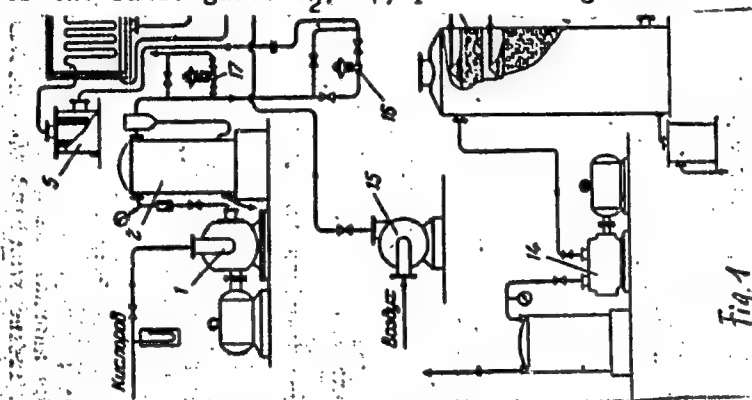
of the initial gas was determined: $C_2H_4 = 3\%$, $O_2 = 0.8\%$; $CO = 13.8\%$; $H_2 = 6.7\%$; $CH_4 = 62\%$; $N_2 = 13.7\%$. For stabilizing the flame, 3% of the total oxygen (79 to 98% of O_2) was required. The temperature of the reaction channel was approximately $1350^\circ C$, that of the reactor block $100^\circ C$. The total time of reaction was 5000 hr, ratios $[O_2] : [CH_4 + 2C_2H_4] = 0.62$ to 0.72 . Optimum yield of $C_2H_2 = 7.3\%$, its average = 6.9% ; total cracking = approximately 30%, effective cracking approximately 30%. The adiabatic temperatures of the reaction were lower than that of the hydrogen formation according to $CO + H_2O = CO_2 + H_2$. The temperature of preheating ($500^\circ C$) probably causes a reduction in O_2 consumption by 10%. The method is suited for supplementing the production of nitrogen fertilizers for which hydrogen is obtained from coke oven gases. A percentage of approximately 4 t of NH_3 per t of C_2H_2 was obtained. There are 3 figures, 2 tables, and 6 references: 4 Soviet-bloc and 2 non-Soviet-bloc. ✓

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Problems of apparatus design for...

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Legend to Fig. 1: basic diagram of a semi-industrial plant for the thermo-oxidative pyrolysis of hydrocarbon gases, 1) compressor XK-3 (KhK-3); 2) receiver-water separator, 3) oven for preheating gas 4) compressor PYT (RUTT), 5) cloth filter, 6) mixer, 7) burner, 8) reaction vessel, 9) carbon black separator, 10) water seal, 11) bunker for carbon black (coke), 12) centrifugal pump, 13) scrubber, 14) gas pump FMK-4 (RMK-4), 15) air pump, 16) regulator for the ratio gas: O₂, 17) pressure regulator.

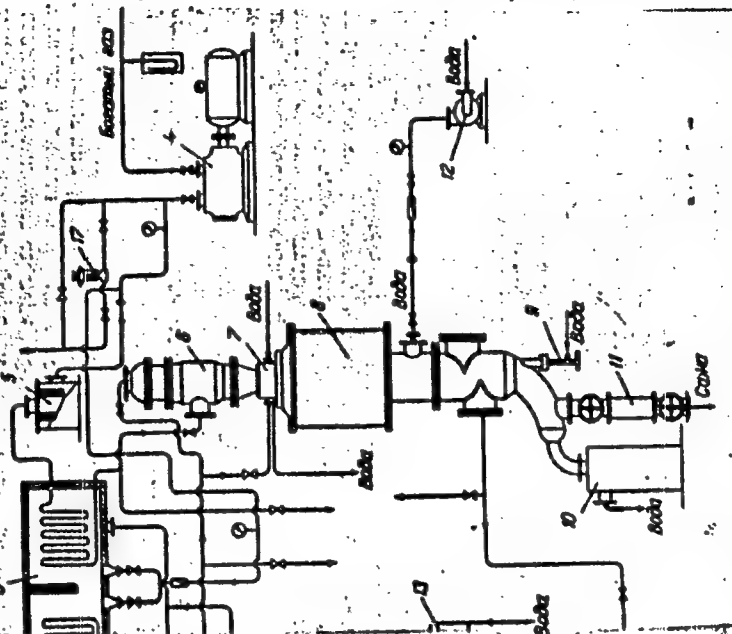


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Probelms of apparatus design for...

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B110/B215

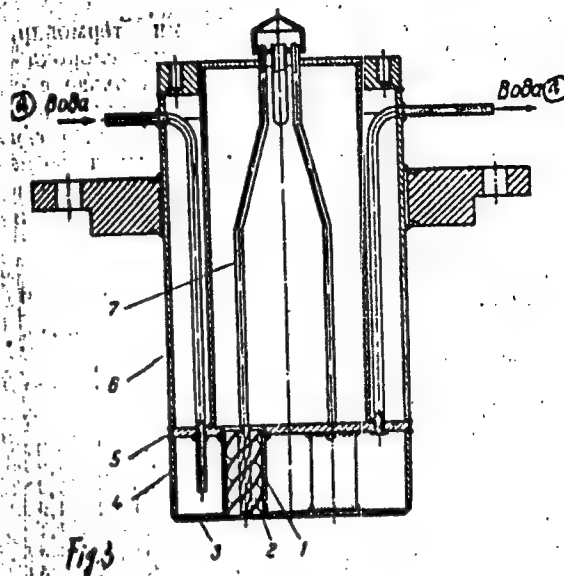
Card 6/7



Problems of apparatus design for...

S/064/61/000/001/002/011
B110/B215

Legend to Fig. 3: triplal burner,
1) socket, 2) whirl spiral,
3) bottom of burner, 4) shell,
5) partition, 6) burner housing,
7) tube for stabilization oxygen,
a) water.



Card 7/7

SEMENOV, V.P.; KAZARNOVSKIY, Ya, S.; KOLODEYEV, I.P.; LITVINCHUK, V.A.

Processing of heavy petroleum residues into synthesis gas. Gaz.
prom. 6 no.2:41-48 '61. (MIRA 14:4)

(Gas manufacture and works)

S/081/61/000/020/083/089
B110/B147

AUTHORS: Semenov, V. P., Kazarnovskiy, Ya. S., Kolodeyev, I. P.,
Litvinchuk, V. A.

TITLE: Conversion of heavy petroleum residues into synthesis gas

PERIODICAL: Referativnyy zhurnal. Khimiya, no. 20, 1961, 405-406,
abstract 20M103 (Gaz. prom-st', no. 2, 1961, 41-48)

TEXT: Experiments on the conversion of mazout into synthesis gas were conducted on an experimental plant (diagram given) for conversion at high temperature. The efficiency of the plant was 6.6-7.9 kg of mazout per hr. The average ratio of the linear velocities of mazout escape from the nozzle and of the vapor-oxygen mixture was ~ 200 , the volume of the reaction space was 0.006 m^3 , the temperature in the reaction zone was $1350-1450^\circ\text{C}$, and the linear velocity of converted gas in the reaction zone was 6-9 m/sec. Experimental and calculated equilibrium compositions of the reaction mixture, and comparative tables of efficiency with respect to carbon or oxygen, calculated from equations and obtained from the values of material equilibrium, are presented. It is concluded that

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Conversion of heavy petroleum...

S/081/61/000/020/083/089
B110/B147

the equations indicated for the techniques of commercial gas production
from carbon raw material have a universal character. [Abstracter's note:
Complete translation.]

Card 2/2

KAZARNOVSKIY, Ya.S.; OVCHARENKO, B.G.; SEMENOV, V.P.; DEREVYANKO, I.G.

Process gas obtained by the high temperature conversion of hydrocarbon gases. Gaz.prom. 7 no.1:43-50 '62. (MIRA 15:1)
(Gas, Natural) (Gas manufacture and works)

KAZARNOVSKIY, Ya.S.; KARKHOV, N.V.; KABANOV, F.I.; OVCHARENKO, B.G.

Production of synthesis gas by high temperature conversion of
hydrocarbon gases at high pressure. Khim.prom. no.6:396-404 Je
'62. (MIRA 15:11)
(Hydrocarbons) (Water gas)

KABANOV, F.I.; KARKHOV, N.V.; KAZARNOVSKIY, Ya.S.; OVCHARENKO, B.G.;
Prinimal uchastiye: ZUYEV, V.I.

Production of process gas by the high temperature conversion
of natural gas at elevated pressure. Khim.prom. no.9:547-555
Ag '62. (MIRA 15:9)

(Gas, Natural)
(Gas manufacture and works)

~~KAZARNOVSKIY, Ya.S.~~; KAZARNOVSKAYA, D.B.; SIDOROV, I.P.

Equilibrium of homogeneous gas mixture reactions at high
pressure. Khim.prom. no.10:747-750 0 '62. (MIRA 15:12)

(Gases)

(Chemical equilibrium)

KAZARNOVSKAYA, D. B.; SIDOROV, I. P.; KAZARNOVSKIY, Ya. S.

Determination of the compressibility of methanol, carbon
monoxide-hydrogen and carbon monoxide-hydrogen-methanol
mixtures at high temperatures and pressures. Khim. prom.
no.3:205-211 Mr '63. (MIRA 16:4)

| | | |
|------------|-------------------|------------|
| (Methanol) | (Carbon monoxide) | (Hydrogen) |
| | (Compressibility) | |

KAZARNOVSKIY, Ya.S.; KAZARNOVSKAYA, D.B.; SIDOROV, I.P.

Equilibrium of the reaction of methanol synthesis from carbon
monoxide and hydrogen at high pressure. Khim. prom. no.6:
426-433 Je '63. (MIRA 16:8)

(Methanol) (Carbon monoxide) (Hydrogen)

MIKHAYLOVA, S.A.; KAZARNOVSKIY, Ya.S.; KAZANOVSKAYA, D.B.

Thermodynamic properties of gaseous methanol at high
temperatures and pressures. Khim. prom. no.4:244-249
Ap '63. (MIRA 16:8)

KAZARNOVSKIY, Ya. S.; MIKHAYLOVA, S. A.; KAZARNOVSKAYA, D. B.

Influence of pressure on the thermal effect of the synthesis
of methanol from carbon oxide and hydrogen. Khim prom no. 3:
183-187 Mr '64. (MIRA 17:5)

ALEYNOV, D.P.; KAZARNOVSKIY, Ya.S.

Production of acetylene by the thermal oxidative pyrolysis of
hydrocarbon gases at elevated pressure. Khim. prom. no.5:332-
339 My '64. (MIRA 17:9)

AIEYNOV, D.P.; KAZARNOVSKIY, Ya.S.

Effect of pressure on the mechanism of the formation and decomposition of acetylene in the thermo-oxidative pyrolysis of methane.
Khim. prom. no.6:422-425 Je '64. (MIRA 18:7)

1. The first part of the document is a list of names and titles of the members of the committee.

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Card 2

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ACCESSION NR: AF5007155

SUBMITTER: M. H. H.

ENCL: 10

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NO REF SOV: 000

OTHER: 000

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Card 2/2

L 40702-65

RM/31/31

EPA/EPF(c)/EPA/EPA(s)-2/ETP(j)/EPA(c)/ETP(m)

Pe-4/Pr-4/Pr-4/Pr-4

ACCESSION NR. AF5010546

UR/0064/65/000/004/0001/0006

AUTHOR: Aleynova, L. N.; Aleynov, D. P.; Kazarnovskiy, Ya. S.; Kornilov, P. P.

TITLE Intermediate stages of partial combustion of methane with oxygen

SOURCE: Khimicheskaya promyshlennost', no. 4, 1965, 1-6

TOPIC TAGS: methane, combustion, kinetics, pyrolysis, combustion mechanism, partial combustion, acetylene

ABSTRACT: Partial methane combustion by thermooxidative pyrolysis is the basic process in the production of synthesis gas or acetylene from natural gas. The kinetics of partial methane oxidation at lower temperatures have been studied extensively by Semenov and co-workers. However, the mechanism proposed in these studies holds only at temperatures below 1000C and cannot be applied to high temperature processes. Experiments were made with oxygen and natural gas in a flow reactor to determine the concentration of intermediates and reaction products (CO, acetylene, ethylene, ethane, propane, O₂, CO, H₂) as a function of methane conversion. Runs were made at initial gas temperatures of 25C and 450C and pressures of 1 and 4 atm. The general trend in the accumulation of intermediates was identical in both experiments. The results indicate that partial oxidation at high temperatures takes place in three stages: 1) methane oxidation, during which oxygen is

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L 40702-65

ACCESSION NR: AP5010546

used for conversion to CO, H₂, H₂O, and CO₂ while the acetylene accumulation remains low (0—0.65 conversion); 2) acetylene accumulation, during which the concentrations remain constant (0.65—0.9 conversion), and 3) cracking of acetylene, characterized by conversion to CO and H₂. The thermal effect is

ASSOCIATION: none

SUBMITTED: 00

ENCL: 00

SUB CODE: FF

NO REF SOV: 015

OTHER: 014

ATT PREP: 3231

Cord 2/2/4

ADAMS, W. L. R.; ADAMS, D. L.; ADAMS, D. L.; ADAMS, D. L.

Intermediate stages of the incomplete oxidation of methane in
oxygen. Khim. prom. 41 no. 4:1-6 A, 195.

(MIRA 18:3)

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